

U.S. Serial Number: 10/678,693  
Reply to Office Action of: July 12, 2006  
Family Number: P2002J099 (JK-0329)

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Page 2 of 8

### LISTING OF THE CLAIMS

This listing of the claims will replace all prior versions and listings of claims in the application.

1 - 14. (Canceled)

15. (Currently Amended) An integrated process for dewaxing a raffinate feedstock containing at least 7270 wppm and up to 20,000 ppmw sulfur and up to 1000 ppmw nitrogen which consists essentially of: (a) contacting the feedstock without prior hydrotreatment with a dewaxing catalyst consisting essentially of ZSM-48 under hydrodewaxing conditions, said dewaxing catalyst including a metal hydrogenation component which is at least one Group 6 metal, at least one Group 8-10 metal, or mixtures of Group 6 and Group 8-10 metals, to form a hydrodewaxed product, and (b) passing at least a portion of the hydrodewaxed product and gaseous components from step (b) without disengagement to a hydrofinishing zone ~~containing a MCM-41 catalyst~~ and hydrofinishing the hydrodewaxed product under hydrofinishing conditions.

16. (Original) The process of claim 15 wherein the metal hydrogenation component is Pt, Pd or mixtures thereof.

17. (Original) The process of claim 15 wherein the hydrodewaxing conditions include a temperature of 360 to 425°C, hydrogen pressures of from 2859-20786 kPa, liquid hourly space velocities of 0.1 to 10 LHSV and hydrogen treat gas rates of from 53.4-1780 m<sup>3</sup>/m<sup>3</sup>.

18. (Original) The process of claim 15 wherein the hydrofinishing conditions include temperatures of 150-350°C, pressures of 100-3000 psig (790-20786 kPa), LHSV of 0.1-20, and treat gas rates of 300-10000 scf/bbl (53-1780 m<sup>3</sup>/m<sup>3</sup>).

U.S. Serial Number: 10/678,693  
Reply to Office Action of: July 12, 2006  
Family Number: P2002J099 (JK-0329)

Page 3 of 8

19. (Cancelled)

20. (Currently Amended) An integrated process for dewaxing a raffinate feed which consists essentially of:

- (a) solvent dewaxing the raffinate to form a raffinate and a slack wax,
- (b) deoiling the slack wax to produce a foots oil,
- (c) in a first reactor contacting the foots oil with a hydrotreating catalyst under hydrotreating conditions to produce a hydrotreated foots oil and gaseous nitrogen- and sulfur-containing contaminants,
- (d) passing at least a portion of the hydrotreated foots oil and gaseous sulfur- and nitrogen-containing contaminants from step (c) without disengagement to a second reactor containing a hydrodewaxing zone that consists essentially of a ZSM-48 dewaxing catalyst and hydrodewaxing the hydrotreated foots oil under hydrodewaxing conditions, said dewaxing catalyst including a metal hydrogenation component which is at least one Group 6 metal, at least one Group 8-10 metal, or mixtures of Group 6 and Group 8-10 metals to form from a hydrodewaxed product, and
- (e) passing at least a portion of the hydrodewaxed product from step (d) without disengagement to a hydrofinishing zone containing a MCM-41 hydrofinishing catalyst and hydrofinishing under hydrofinishing conditions.

U.S. Serial Number: 10/678,693  
Reply to Office Action of: July 12, 2006  
Family Number: P2002J099 (JK-0329)

Page 4 of 8

21. (Original) The process of claim 20 wherein the hydrotreating conditions temperatures of 315-425°C., pressures of 2170-20786 kPa, Liquid Hourly Space Velocities (LHSV) of 0.1-10 and hydrogen treat rates of 89-1780 m<sup>3</sup>/m<sup>3</sup>.

22. (Original) The process of claim 20 wherein the metal hydrogenation component is Pt, Pd or mixtures thereof.

23. (Original) The process of claim 20 wherein the hydrodewaxing conditions include a temperature of 360 to 425°C., hydrogen pressures of from 2859-20786 kPa, liquid hourly space velocities of 0.1 to 10 LHSV and hydrogen treat gas rates of from 53.4-1780 m<sup>3</sup>/m<sup>3</sup>.

24. (Canceled)

25. (Currently Amended) The process of claim 20 wherein the slack wax or foots oil is blended with raffinate feed prior to step G (c).

26 – 37. (Canceled)

38. (New) The process of claim 15, wherein the hydrofinishing zone contains a MCM-41 hydrofinishing catalyst.

39. (New) The process of claim 20, wherein the hydrofinishing zone contains a MCM41 hydrofinishing catalyst.